

UK Patent Application GB 2 385 009 A

(43) Date of A Publication 13.08.2003

(21) Application No 0302831.3

(22) Date of Filing 07.02.2003

(30) Priority Data

(31) 60356108 (32) 11.02.2002 (33) US
(31) 60425377 (32) 12.11.2002

(51) INT CL⁷

B01D 17/02 // B01D 17/032

(52) UK CL (Edition V)
B1D DPJA

(56) Documents Cited
GB 2242373 A
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WO 2001/071158 A1

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(58) Field of Search

UK CL (Edition V) B1D DACA DPGA DPMX DPNA
DPOA
INT CL⁷ B01D 17/032 17/06
Other: Online: WPI, EPODOC, JAPIO

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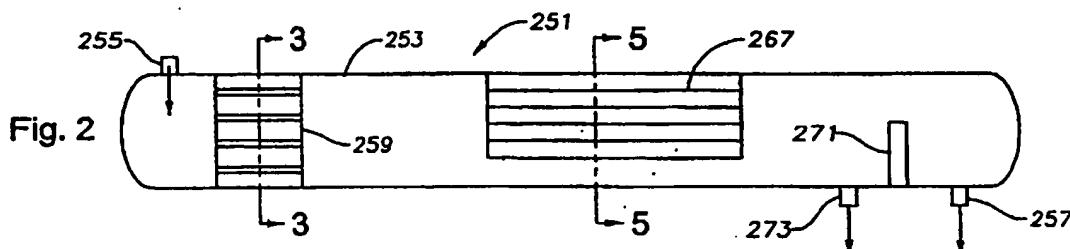
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(54) Abstract Title

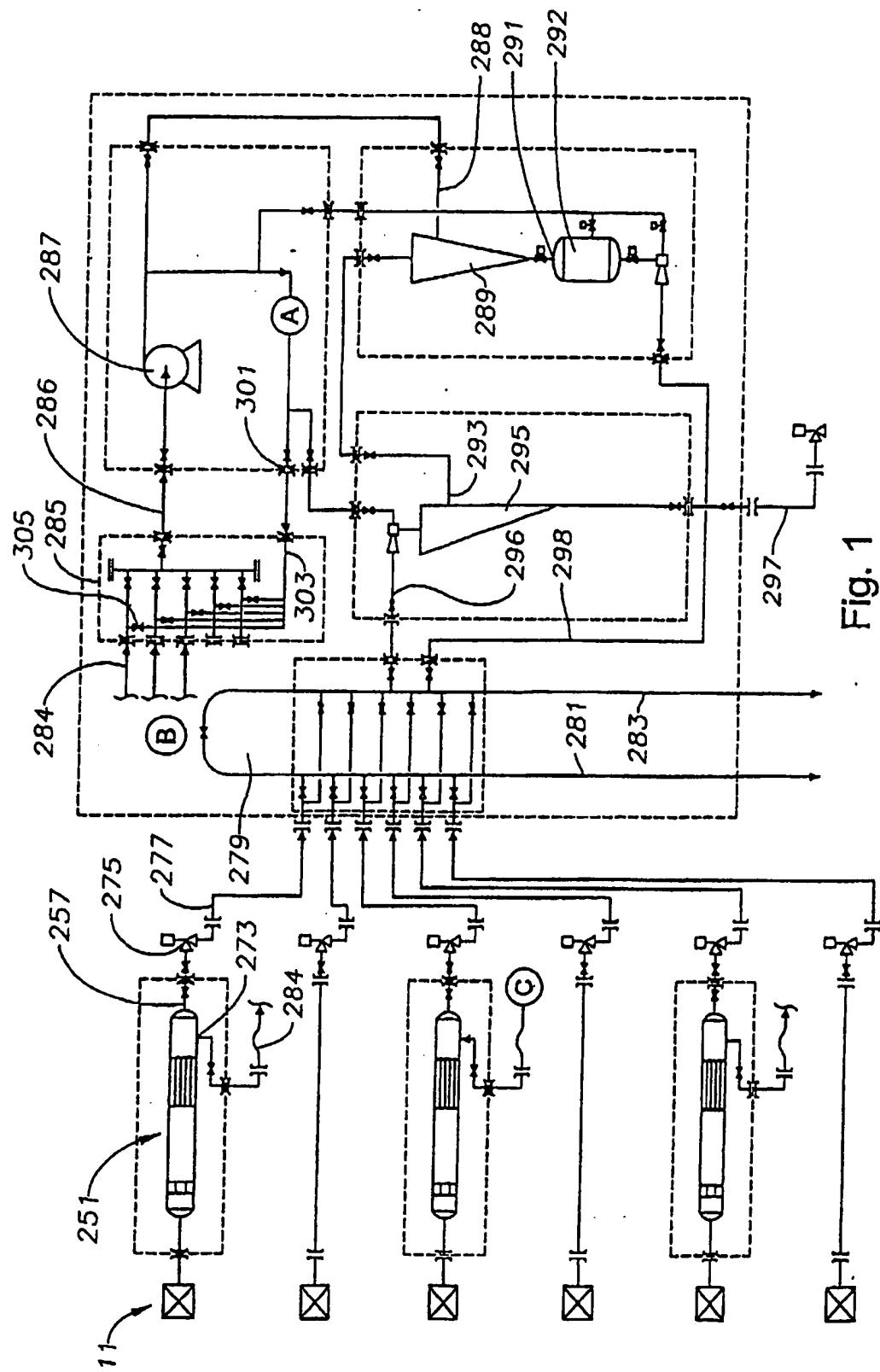
A subsea well fluid processing system

(57) A subsea well fluid separator 251 for separating heavy and light components of well fluid flowing from a subsea well (11, Fig 1) and directing the lighter components to flow to a surface processing facility, and a choke (275, Fig 1) located downstream of the separator for limiting the flow rate of well fluid from the subsea well. Preferably the separator has a cylindrical chamber and a coalescing unit 259 having a plurality of tubes to which an electrical potential is applied is located within. A dielectrophoresis unit 267 having a pair of sheets spaced close to each other and to which an electric potential is supplied may be located in the chamber downstream of the coalescent unit 259. Advantageously a number of separators make up a system for separating the heavy and light components into their respective outlets and a pump (287, Fig 1) connected to the outlet of the heavy component 257 transfers the component through flowlines (281, 283, Fig 1) to a disposal location or is recirculated for backflushing purposes.



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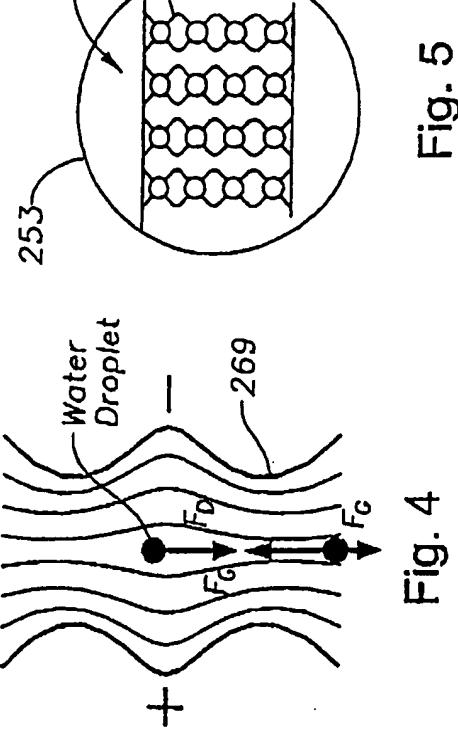
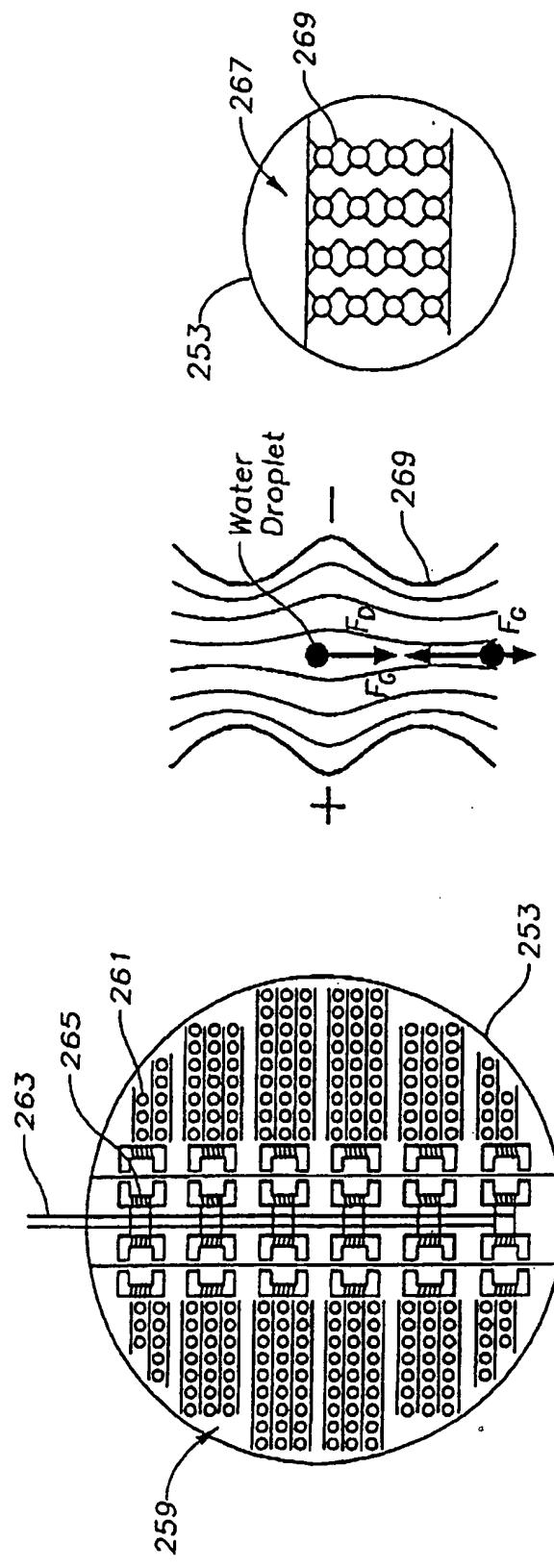
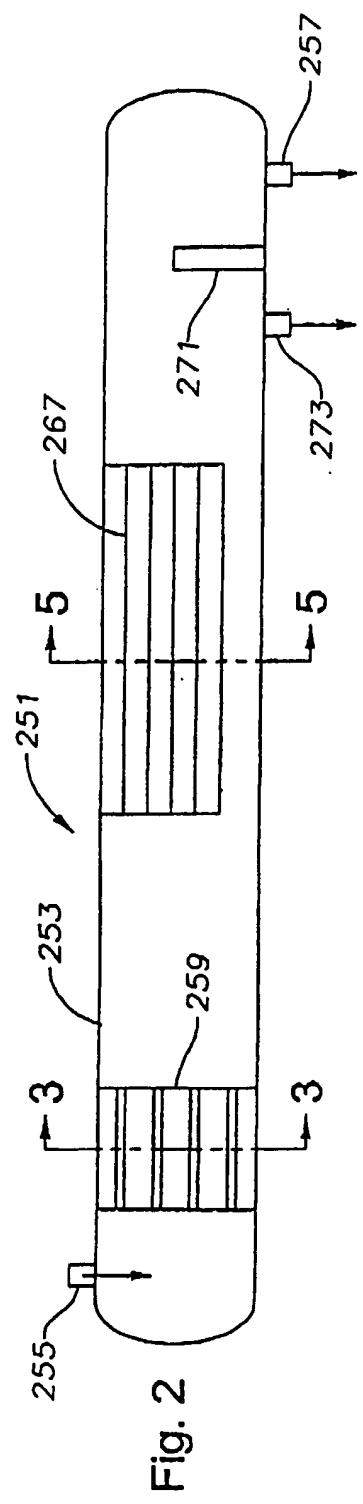


Fig. 5

Fig. 3

Fig. 4

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SUBSEA PRODUCTION SYSTEM

~~This application claims the provisional application Serial No. 60/356,108, filed February 11, 2002 and provisional application Serial No. 60/425,377, filed November 12, 2002.~~

5 FIELD OF THE INVENTION

This invention relates in general to well fluid processing systems and in particular to a subsea system.

BACKGROUND OF THE INVENTION

Oil and gas wells typically produce a well fluid that requires separation to remove formation water from the flow stream. With subsea wells, the separation typically takes place on a production platform or vessel. This usually requires pumping the well fluid, including the formation water, to the surface production facility. In deep water installations, thousands of feet deep, the energy required to pump the water is extensive.

Locating the separation unit subsea has been proposed and done on at least one occasion. The environment of a subsea separation unit and a surface unit differs because of the high hydrostatic forces imposed on the separation vessels. While vessels can be made stronger, generally this results in a larger size and weight. Larger size and weight increase the difficulty of deploying the units.

Also, separators commonly require maintenance because of sand accumulation and mineral deposits on the components. Once installed subsea, maintenance becomes difficult because of the sea depths. Further, shutting down a separation system for maintenance would normally require shutting off well flow, which is expensive.

SUMMARY OF THE INVENTION

In this invention, a choke located downstream of the separator for limiting the flow rate of well fluid from the subsea well. The placement of the choke allows higher operating pressures in the separator, which facilitates separation. The

separator has a cylindrical chamber, preferably with a length at least ten times its diameter. A coalescing unit having a plurality of tubes to which an electrical potential is applied is located in the chamber to cause water droplets in the well fluid flowing through the tubes to coalesce into larger droplets. Also, preferably a dielectrophoresis 5 unit is located in the chamber downstream of the coalescent unit. The dielectrophoresis unit has a pair of undulating sheets spaced close to each other, the sheets being supplied with an electrical potential to force the water droplets in the well fluid into predetermined passage portions between the sheets to form high water content sections of liquid.

10 In the preferred embodiment, the system has a number of separators for separating heavier and lighter components of well fluid, each of the separators having a heavier component outlet and a lighter component outlet. A pump has an intake connected to each of the heavier component outlets of the separators. A disposal line is connected to an outlet of the pump and leads to a disposal location for pumping the 15 heavier components to the disposal location. Bypass conduits are connected between the outlet of the pump and the heavier component outlets of the separators. When actuated, bypass valves in the bypass conduits cause at least some of the heavier components being pumped by the pump to flow back into the heavier component outlet of the one of the separators for backflushing while the heavier components 20 from the other separators continue to flow through the second heavier component line to the inlet of the pump.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 is a schematic of a production system for the wellhead assembly of Figures 1A and 1B.

25 Figure 2 is a schematic sectional view of one of the separators shown in Figure 1.

Figure 3 is an enlarged schematic sectional view of the separator of Figure 2, taken along the line 31-31 of Figure 2, illustrating the coalescence separator portion.

30 Figure 4 is an enlarged schematic view of a dielectrophoresis separator portion of the separator of Figure 2.

Figure 5 is an enlarged schematic sectional view of the separator of Figure 2, taken along the line 33-33 of Figure 2, illustrating the dielectrophoresis separator portion.

DETAILED DESCRIPTION OF THE INVENTION

5 Figure 1 illustrates schematically a subsea processing system for the various wells 11 within a field. The subsea processing systems separates water and sand. The system includes a plurality of separators 251. A single separator 251 may be utilized with each subsea well assembly 11, or more than one well 11 may feed into a separator 251. Separator 251, as shown in Figure 2, comprises a horizontal vessel 253
10. that locates on the sea floor. Generally, greater water depths will require a higher wellhead pressure with corresponding lower actual gas volumes when separation takes place at the sea floor. Lower gas volumes are beneficial for oil/water separation because fewer gas bubbles will move vertically and disturb the horizontal flow pattern generated by the oil and water flowing through the separator vessel 253. The low gas
15 percentage also allows more of the separator vessel to be utilized for oil/water separation.

In addition to the issue described above, higher pressure in itself within separator vessel 253 will impact the separation. Preliminary results show that separation occurs easier at higher pressures. This can be cause by the fact that high
20 pressure causes the liquid hydrocarbon fraction to be lighter, hence increase the density difference between water and oil. The oil fraction becomes lighter because lighter hydrocarbon fractions are liquefied at the higher pressure, hence if combined with the heavier fractions, the combination can reduce the overall density of the liquid hydrocarbon phase. Separator vessel 253 is designed to withstand the high external
25 pressure due to the very deep water. Also, conservative design does not allow one to reduce the designed pressure differential due to internal pressure. Generally, smaller diameters will give thinner wall thickness for the same external pressure. For example, a 2.8 meter diameter cylinder requires 140 millimeters wall thickness to withstand a selected pressure. A 2.5 meter diameter cylinder will withstand the same
30 pressure with a wall thickness of 25 millimeters. Consequently, separator 253 has a relatively small diameter, preferably no more than 1/10th its length.

Separator 251 may be of various types for separating water and oil. In this embodiment, separator 259 employs a coalescent unit 259. Coalescent unit 259 has a plurality of passages 261 within it. Figure 3 shows the large number of separate passages 261 located within vessel tubes 53. An electrostatic field is applied to the oil and water mixture at the tubes or passages 261. By exposing the mixture of water and oil to an electrostatic field, the dipolar water droplets contained in the oil phase will be oriented in a way that makes them collide or coalesce with each other. This causes the water droplets to grow to bigger droplets. Generally, bigger droplets move and separate faster than smaller droplets. Consequently, a first separation from water and oil takes place in coalescent unit 259. This reduces the required retention time to get the water content out of the oil produced, allowing the separator vessel 253 diameter/size to be reduced.

As shown in Figure 3, preferably low voltage supplied subsea is routed through low voltage wires 263 into the interior of separator vessel 253. A plurality of 15 transformers 265 transform the low voltage to high voltage that is required for providing the electrostatic field. The same low voltage power supply is utilized for other functions, such as operating the solenoids and sensors involved with control of each subsea well 11.

If coalescent unit 259 is not adequate to reach the desired water content, a 20 second stage could be employed. A second stage could be another coalescent unit 259 or it could be a unit of a different type, such as dielectrophoresis unit 267. Unit 267 also uses an electrostatic field, however the field is configured to force the water droplets into designated sections of the separator and thereby form streams of water. Electrode sheets 269, as shown in Figures 4 and 5, have undulations. Electrode sheets 25 269 are closely spaced and arranged with the constrictive portions where two valleys are separated by the widened portions where two peaks are spaced across from each other. Sheets 269 force the water droplets to move towards the stronger section of the electrostatic field with stronger field gradients. The forces imposed by the gradient field are in the order of magnitude two to five times greater than the gravity force. 30 This phenomenon is used to guide the water droplets into these predetermined sections, where they form continuous sections of water for use in separation.

Dielectrophoresis unit 267 reduces the time normally needed for a conventional gravity separator.

Referring again to Figure 2, a bulkhead 271 extends upward from separator vessel 253 near its downstream end. Bulkhead 271 divides a section for collecting 5 higher water concentrations. A water outlet 273 is located upstream of bulkhead 271. Oil and water inlet 255 is located on an upper side of the upstream end of separator vessel 253. Oil outlet 257 is located on the downstream end of separator vessel 253 on the lower side.

Referring back to Figure 1, a choke 275 is located downstream of oil outlet 10 257. Choke 275 is a conventional device that provides a variable orifice for increasing pressure upstream and decreasing flow. One of the chokes 275 is typically located on the tree of each of the subsea wells 11. Choke 275 is adjusted to create a higher pressure within separator 251 to enhance separation, as previously mentioned.

A flowline jumper 277 connects choke 275 to manifold 279. Choke 275 could 15 be incorporated as part of flowline jumper 277 such that it is lowered and installed with jumper 277. Alternately, choke 275 could be mounted to manifold 279.

Manifold 279 is a conventional unit that has a pair of lines 281 and 283 that lead to the surface for delivery of the separated oil and any entrained gas therein. All of the various separators 251 lead to manifold 279.

20 The separated water outlet 273 connects to a flowline 284, which leads to a valving module 285. The various flowlines 284 join each other in module 285, with the combined flow leading to an intake line 286 of a subsea pump 287. Flowlines 281 and 283 lead back to a surface processing unit for transporting the oil. Water pump 287 discharges through a line 288 into a vortex separator 289. Vortex separator 289 25 has an output 291 that leads back to an injection well for injecting the separated water. The output is a mixture of water and in many cases of sand that has been produced from the formation. The higher content of sand flows through output line 291. The free water 293 flows back to a second separator 295 that leads to flowline 291 for injecting into a well. The second vortex separator 295 separates any remaining oil 30 from the water and delivers the oil through line 296 back to manifold 279 for commingling with the other oil being produced through lines 281 and 283. Similarly, any oil washed from the sand and sand collection vessel 292 is filtered and returned

via line 298 to manifold line 283. Vortex separator 289 thus separates sand from liquid, while vortex separator 295 separates any remaining oil from the water.

A valve 301 is connected to a line 303 that leads from the output of pump 287. Line 303 branches into separate lines, each connected to one of the lines 284 leading from one of the separators 251. Each line has a valve 305. Opening valves 301 and 305 enables water to flow backwards through one of the water outlet lines 284 into the water outlet 273 for backflushing. Sand and other deposits accumulate in the subsea separation vessel 253. These sands and/or deposits are removed from separator 251 by the backflushing injection through line 284. The injection of water creates turbulence within separator vessel 253 to cause the sand and other deposits to flow out with the produced oil out manifold lines 281 and 283.

The invention has significant advantages. Locating the choke downstream of the separator allows higher operating pressures in the separator. The combination of a coalescence unit and a dielectrophoresis unit within a small diameter separators provides a compact subsea processing unit. The backflushing capability reduces maintainence.

While the invention has been shown in only one of its forms, it should be apparent to those skilled in the art that it is not so limited but is susceptible to various changes without departing from the scope of the invention.

Claims:

1. A subsea well fluid processing system, comprising:

a subsea well fluid separator for separating heavier and lighter components of well fluid flowing from a subsea well and directing the lighter components to flow to a surface processing facility; and

5 a choke located downstream of the separator for limiting the flow rate of well fluid from the subsea well.

2. The system according to claim 1, wherein the separator comprises:

10 a cylindrical chamber having a length at least ten times its diameter.

3. The system according to claim 1, wherein the separator comprises:

a coalescing unit having a plurality of tubes to which an electrical potential is applied to cause water droplets in the well fluid flowing through the tubes to coalesce 15 into larger droplets; and

a dielectrophoresis unit having a pair of undulating sheets spaced close to each other, the sheets being supplied with an electrical potential to force the water droplets in the well fluid into predetermined passage portions between the sheets to form high water content sections of liquid.

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4. The system according to claim 3, wherein the dielectrophoresis unit is located downstream from the coalescing unit within the separator.

5. A subsea well fluid processing system, comprising:

25 first and second separators for separating heavier and lighter components of well fluid, each of the separators having a heavier component outlet and a lighter component outlet;

a lighter component line connected to the lighter component outlet of each of the separators for delivering the lighter components to a surface processing facility;

first and second heavier component lines connected to the heavier component outlets of the first and second separators, respectively;

5 a pump having an intake connected to each of the heavier component outlets;

 a disposal line connected to an outlet of the pump and leading to a disposal location for pumping the heavier components to the disposal location;

 first and second bypass conduits connected between the outlet of the pump and to the first and second heavier component outlets of the separator, selectively; and

10 a first and second bypass valves in the first and second bypass conduits, respectively, such that opening the first bypass valve and closing the second bypass valve causes at least some of the heavier components being pumped by the pump to flow back into the heavier component outlet of the first separator for backflushing while the heavier components from the second separator continue to flow through the second heavier component line to the inlet of the pump.

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6. The system according to claim 5, further comprising a choke located downstream of each of the separators for limiting the flow rate through the separators.

20 7. The system according to claim 5, wherein each of the separators comprises:

 a cylindrical chamber;

 a coalescing unit in the chamber, having a plurality of tubes to which an electrical potential is applied to cause water droplets in the well fluid flowing through the tubes to coalesce into larger droplets; and

25 a dielectrophoresis unit in the chamber, having a pair of undulating sheets spaced close to each other, the sheets being supplied with an electrical potential to force the water droplets in the well fluid into predetermined passage portions between the sheets to form high water content sections of liquid.

8. The system according to claim 7, wherein the dielectrophoresis unit is located downstream from the coalescing unit within the separator.

9. A method of processing well fluid from a subsea well, comprising:

5 (a) deploying a well fluid separator subsea and connecting an inlet of the separator to the well;

(b) connecting a choke downstream of the separator;

(c) flowing well fluid from the well to the inlet of the separator, and limiting the flow rate of the well fluid with the choke; and

10 (d) with the separator, separating heavier and lighter components of well fluid flowing from a subsea well and directing the lighter components to flow to a surface processing facility.

10. The method according to claim 9, wherein step (d) comprises:

15 applying an electrical potential to a plurality of tubes to cause water droplets in the well fluid flowing through the tubes to coalesce into larger droplets; and

applying an electrical potential to a pair of undulating sheets spaced close to each other to force the water droplets in the well fluid into predetermined passage portions between the sheets to form high water content sections of liquid.

20

11. The method according to claim 10, wherein the tubes are located upstream of the sheets.

12. A method of processing well fluid from first and second subsea wells,

25 comprising:

(a) with a first separator, separating heavier and lighter components of well fluid flowing from the first well;

(b)with a second separator, separating heavier and lighter components of well fluid flowing from the second well;

(c)delivering the lighter components of each of the separators to a surface processing facility;

5 (d)delivering the heavier components from a heavier component outlet of each of the separators to a pump;

(e)with the pump, delivering the heavier components to a disposal location; and

(f)selectively, causing at least a portion of the heavier components being 10 pumped by the pump back to the heavier component outlet of the first separator to backflush the first separator while continuing receive heavier components from the heavier component outlet of the second separator.

13. The method according to claim 12, further comprising:

15 ceasing step (f) and causing at least a portion of the heavier components being pumped by the pump back to the heavier component outlet of the second separator to backflush the second separator while continuing to receive heavier components from the heavier component outlet of the first separator.

20 14. The method according to claim 13, further comprising:

placing a choke downstream of each of the separators and limiting the flowrate through the separators with the chokes.

15. The method according to claim 14, wherein steps (a) and (b) comprise:

25 applying an electrical potential to a plurality of tubes to cause water droplets in the well fluid flowing through the tubes to coalesce into larger droplets; and

applying an electrical potential to a pair of undulating sheets spaced close to each other to force the water droplets in the well fluid into predetermined passage portions between the sheets to form high water content sections of liquid.

5 16. The method according to claim 15, wherein the tubes are located upstream of the sheets.



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Application No: GB 0302831.3
Claims searched: 1 - 4 & 9 - 11

Examiner: Beverley Lloyd
Date of search: 28 April 2003

Patents Act 1977 : Search Report under Section 17

Documents considered to be relevant:

Category	Relevant to claims	Identity of document and passage or figure of particular relevance	
A	-	GB 2242373 A	(BRITISH) See Figs; lines 9 - 14, page 3; lines 17 - 22, page 4
A	-	WO 01/71158 A1	(KVAERNER) See Figs & description
A	-	FR 2774924 A	(PROCEDES) See Figs & abstract at least

Categories:

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